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#### Title: Biodiesel production as an alternative to reduce the environmental impact of University food courts

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# **INTRODUCTION**







"... implementing the management and adequate disposal of residual animal and/or plant fats and oils, seeking to consider the adoption of management measures, to prevent and reduce environmental impacts and harmful health effects"

NADF-012-AMBT-2015



Figure 2. Green circular economy model of waste cooking oil management.

# METHODOLOGY



**Figure 3.** Reference Framework for a Life Cycle Analysis (LCA). Source: (ISO 14044, 2006) □ Software: SimaPro 9.1.0.11 PhD.

**Ecoinvent** database.

- □ The method was CML-IA baseline C3.06/EU25, with eleven impact midpoint assessment, categories: Abiotic Depletion Potencial (ADP, elements), Abiotic Depletion Potencial (ADP, fossil fuels), Global Warming Potential (100 years) (GWP), Ozone Layer Depletion (ODP), Human Toxicity (HT), Freshwater Aquatic Ecotoxicity (FWAE), Marine Aquatic Ecotoxicity (MAE), Terrestrial Ecotoxicity (TE), Photochemical Oxidation (PO), Acidification (A) and Eutrophication (E). The interpretation, a heterogeneous process (scenario 1) was compared with a homogeneous process (scenario 2), data reported by (Talens et al., 2010) were used for the homogeneous process.
- □ The endpoint impact assessment (Ecosystem Quality, Human Health Damage and Resource Availability) was carried out using the ReCiPe 2016 Endpoint (H) V1.04 / World (2010) H/A.



**Figure 4.** Integral Management System of Organic Waste from University food courts, with alternative scenarios. Source: own study.



**Figure 5.** System boundary for the management of waste cooking oil in the University food courts of the UAEMéx, through a heterogeneous process (scenario 1) or homogeneous process (scenario 2). Source: own study.

#### RESULTS



**Figure 6.** Percentage of consumption by type of oil in the University food courts of the UAEMéx. Source: own study.

**Table 1.** Inventory analysis according to the functional unit (1 L) in biodiesel production with a

#### heterogeneous process.

		Input			Output			
Stage	Flow	Parameter	Amount	Unit	Flow	Parameter	Amount	Unit
Collect	Energy	Gasoline	0.128	tkm	Middle	WCO	1.100	L
	Raw material	WCO	1.100	L	flow			
Pre	Energy	Electricity	0.722	kWh	Middle	WCO	1.100	L
treatment		consumption			flow			
	Raw material	Potable water	0.745	L	Residue	Waste	0.745	L
						water		
		WCO	1.100	L				
Reaction	Energy	Electricity	11.20	kWh	Product	Biodiesel	1.000	L
		consumption						
	Raw material	WCO	1.100	L				
		Pig iron	0.005	kg	Co product	Glycerine	0.100	L
		(Fe <sub>2</sub> O <sub>3</sub> )						
		Lime	0.079	kg	Residue	Waste	0.819	L
		hydraliuc				water		
		(CaO)			Reciclable	Methanol	0.209	L
					product			
		Water,	0.819	L	Reusable	Bifuntional	0.084	kg
		deionised			product	catalysts		
		Methanol	0.232	L		(Fe <sub>2</sub> O <sub>3</sub> /CaO)		

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**Table 2.** Environmental impacts in the collection, pretreatment and heterogeneous reaction stages,using the CML-IA baseline method V3.06/EU25 for 1 L biodiesel.

Impact category	Unit	Collect	Pretreatment	Heterogeneous reaction	TOTAL
ADP				2.94E-05	3.64E-05
(elements)	kg Sb <sub>eq</sub>	5.34E-06	1.72E-06		
ADP	-			105.56	114.93
(fossil fuels)	MJ	3.39	5.98		
GWP	kg CO <sub>2 eq</sub>	0.24	0.46	8.91	9.61
ODP	kg CFC-11 <sub>eq</sub>	3.87E-08	3.46E-08	6.10E-07	6.83E-07
НТ	kg 1,4-DB <sub>eq</sub>	0.06	6.99E-02	1.23	1.36
FWAE	kg 1,4-DB <sub>eq</sub>	2.12E-03	8.18E-03	0.14	0.15
MAE	kg 1,4-DB <sub>eq</sub>	44.50	136.01	2387.89	2568.40
TE	kg 1,4-DB <sub>eq</sub>	4.11E-04	2.47E-03	0.04	0.05
РО	kg $C_2 H_4_{eq}$	9.02E-05	7.91E-05	1.55E-03	1.72E-03
Α	kg SO <sub>2 eq</sub>	1.07E-03	1.96E-03	0.03	3.76E-02
E	kg $PO_{4 eq}$	1.67E-04	1.96E-04	3.45E-03	3.81E-03



**Figure 7.** Percentage contribution of the midpoint impact categories for the heterogeneous process (scenario 1) and the homogeneous process (scenario 2) using the CML-IA baseline method V3.06/EU25. Source: own study.



Figure 8. Endpoint impacts for alternative scenarios using ReCiPe 2016: heterogeneous process (scenario 1) and homogeneous process (scenario 2). Source: own study.

# CONCLUSIONS

- ✓ The type of oil consumed in the University food courts of the UAEMéx is mainly sunflower and is converted into residual oil when subjected to cooking under elevated temperatures; this was the raw material to produce biodiesel under a heterogeneous process. In this regard, this was the raw material to produce biodiesel under a heterogeneous process. The initial environmental load is zero because it is a residue, it should be noted that the impact was not quantified from the stage of cultivation or extraction of the oil, which makes the process studied sustainable.
- ✓ Within the system boundary, it was established that the collection of waste cooking oil had the least contribution in the impacts studied, then the pretreatment stage. In the reaction stage for the heterogeneous process, the energy consumption due to electrical and thermal demands resulted in the greatest environmental impacts in the following categories: abiotic depletion potential (fossil fuels) (105.56MJ), 100-year global warming (8.91 kg CO<sub>2 eq</sub>) and marine water ecotoxicity (2387.89 kg 1.4-DB eq).
- ✓ In the heterogeneous reaction step, the **bifunctional catalyst** (Fe<sub>2</sub>O<sub>3</sub>/CaO) replaces H<sub>2</sub>SO<sub>4</sub> and NaOH, performing in a single step the esterification and transesterification, consuming less electricity at the activation of the catalyst that is at least three times reused without calcining again; methanol is recovered for recycling during the reaction; as for glycerin, it is purified, which gives the process a circular economy approach that ensures the sustainability of biodiesel production.

#### CONCLUSIONS

- ✓ With respect to the end-point environmental impacts, the homogeneous process has greater to human health damage with 1.77 points more than the heterogeneous process. This process is mainly affected by emissions from waste disposal and electricity consumption.
- ✓ The carbon footprint for the heterogeneous process is lower by 82.52% compared to the homogeneous process. This contributes to the mitigation of greenhouse gases and compounds, as it replaces fossil fuels, maintains carbon sinks and prevents deforestation.
- ✓ The identified areas of opportunity were the reduction of electricity consumption using renewable energies such as solar photovoltaics; the environmental sustainability of the process from the energy generated by the production of biodiesel and the energy consumed; the economic and environmental valorization of glycerin.
- ✓ In the University food courts, it is suggested to conduct environmental education campaigns in the collection sites to efficiently perform this stage with a pretreatment (purification of impurities), as well as standardizing a process that allows sampling to verify the initial quality of waste cooking oil and a collection route that guarantees the recycling of waste cooking oil. Finally, it was also concluded that a program of management of waste cooking oil in the UAEMéx should be implemented in order to reduce the carbon footprint of the University food courts.

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